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# Membrane separation of hydrogen applied on various industrial gases



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#### Evaluate

Evaluate membrane separation of H<sub>2</sub> from syngas (H<sub>2</sub>– CO–CO<sub>2</sub>)

#### Study

Study effects of pressure, flowrate, and gas composition

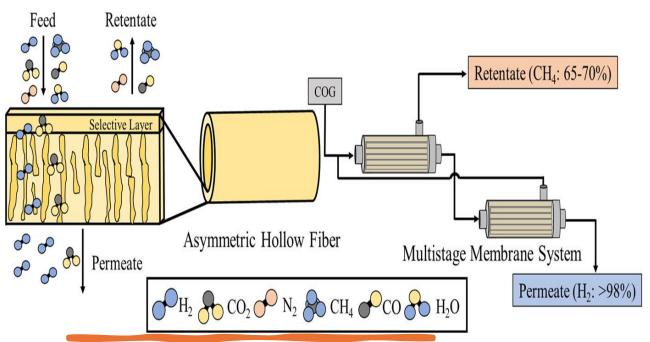
#### Assess

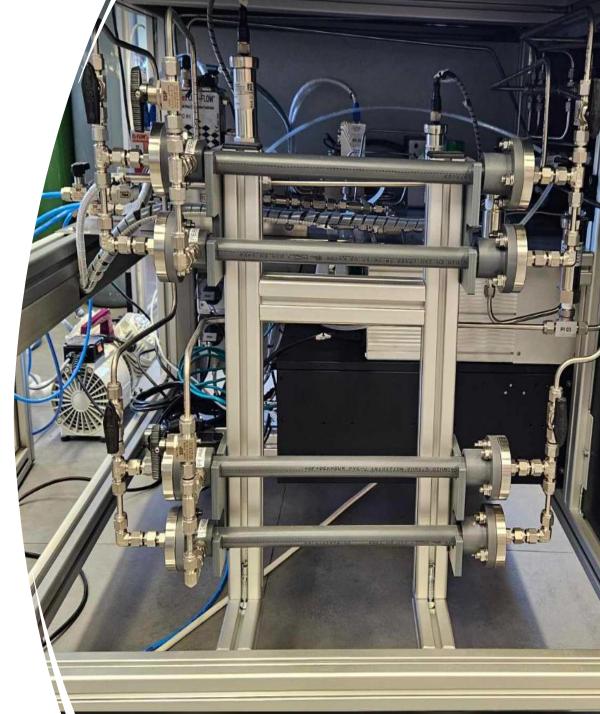
Assess key
performance
metrics: purity,
recovery,
selectivity, stage
cut

#### Provide

Provide insights for industrial hydrogen recovery and purification operations.

#### Schematics of the membrane separator





## Overview of the study

- Feedstock: Hydrogen is usually produced in mixtures with CO and CO<sub>2</sub> → requires purification for clean use.
- Simulation: A synthetic gas mixture of H<sub>2</sub>, CO, and CO<sub>2</sub> with known compositions.
- Process: Separation carried out using a single-stage gas membrane unit at different pressures and flowrates.
- Measurements: Gas composition analyzed in feed and permeate streams using GC.
- Key Analysis: Calculated hydrogen purity, recovery, selectivity, and stage cut for each run using Jupyter Notebook (python).
- **Relevance:** This study provides insight into membrane transport mechanisms and offers a practical demonstration of the potential of membrane separation processes for efficient and scalable hydrogen purification and recovery in industry.

## **Process of Separation**

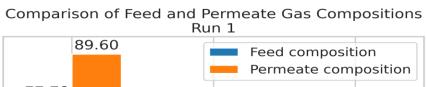
Controlled flowrate of (50–180 L/h) and Pressure (2-8 bar).

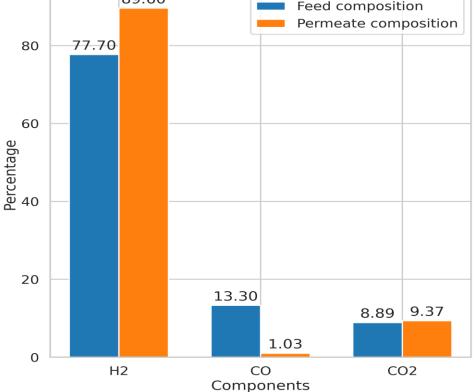
Driving force: pressure difference → H<sub>2</sub> molecules permeate faster due to:

- Lower molecular weight
- Smaller kinetic diameter (~0.29 nm)
- Permeate gas enriched in H<sub>2</sub>, while CO (3.74 nm) and CO<sub>2</sub> (3.33 nm) are retained in the retentate.
- Output streams analyzed using gas chromatography (GC) to determine composition.

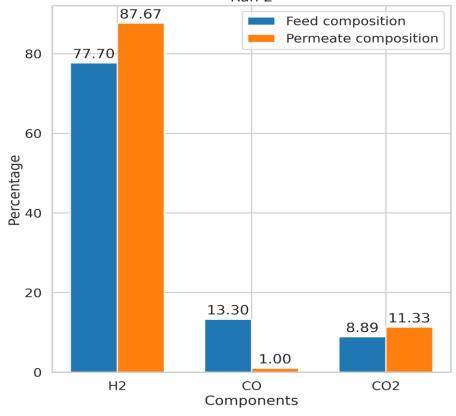
#### Feed composition Range

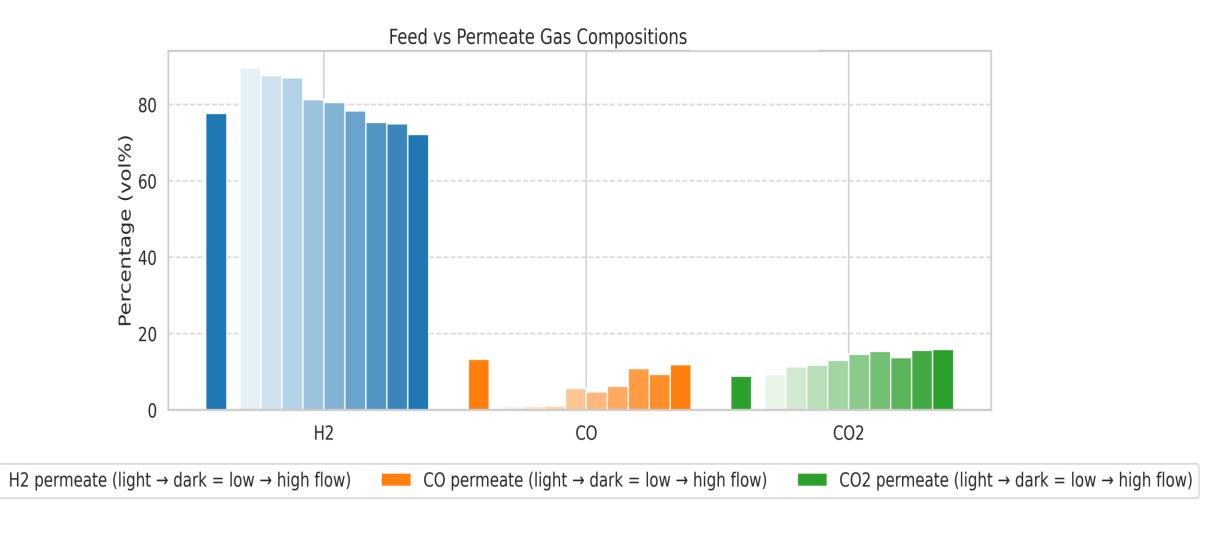
- H<sub>2</sub>: ~55–60%
- CO: ~20–25%
- CO<sub>2</sub>: ~15–20%

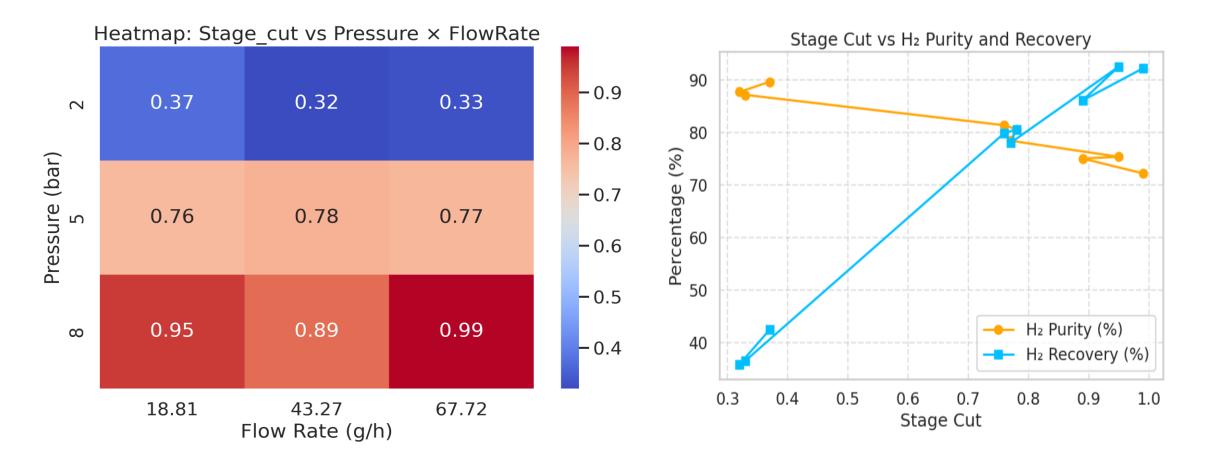


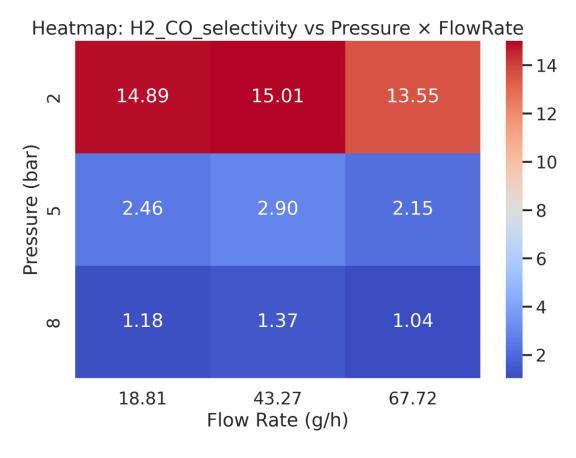


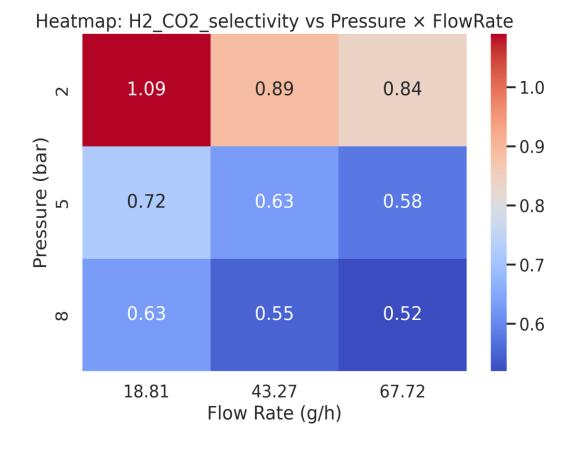




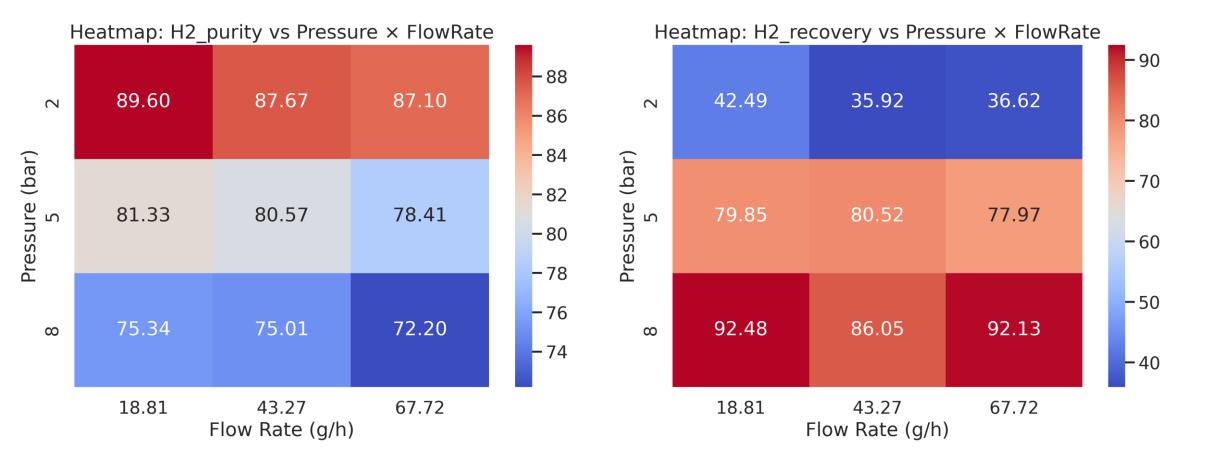












	Pressure	Flow Rate		H <sub>2</sub> _CO_	H <sub>2</sub> _CO <sub>2</sub> _		
Feedstock	(bar(a)	Regime (l/h)	H <sub>2</sub> recovery %	selectivity	selectivity	Stage-cut	Hydrogen purity
Natural Gas	2	50	42.48	14.89	1.094	0.36	89.60
Natural Gas	2	115	35.92	15.00	0.88	0.31	87.67
Natural Gas	2	180	36.61	13.55	0.84	0.32	87.10
Natural Gas	5	50	79.85	2.45	0.71	0.76	81.33
Natural Gas	5	115	80.51	2.89	0.62	0.77	80.57
Natural Gas	5	180	77.96	2.15	0.58	0.77	78.41
Natural Gas	8	50	92.47	1.18	0.62	0.95	75.34
Natural Gas	8	115	86.05	1.37	0.54	0.89	75.01
Natural Gas	8	180	92.12	1.03	0.51	0.99	72.20

### **Key Findings on Gas Separation Performance**

#### H<sub>2</sub> separation performance:

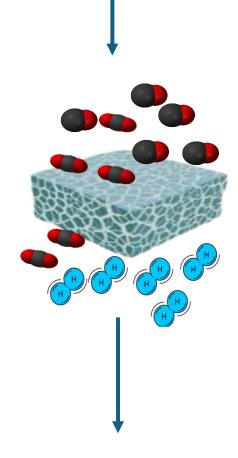
- High purity (up to ~90%) at low pressures and flow rates.
- Purity decreases at higher pressures and stage cuts.

#### Competition from CO and CO<sub>2</sub> against H<sub>2</sub>:

- Partial pressure increase at high pressure drives CO and CO<sub>2</sub> permeation.
- CO<sub>2</sub> shows higher solubility in the membrane → stronger competition.
- At high stage cuts, separation factor decreases → permeate resembles feed.

#### **Overall trade-off:**

- Low stage cut → high purity, low recovery.
- High stage cut → high recovery, lower purity.



## Implications and Conclusion

 $H_2 \rightarrow CO_2 \rightarrow CO$  permeation

- Lower pressure and flowrates enhance hydrogen selectivity, while higher operating conditions increase overall throughput and reduce hydrogen purity.
- Operating conditions must be optimized depending on the application: if purity of hydrogen is highly required (fuel cells), we operate at low stage cut: if high recovery (industrial processes) is priority, we push towards higher stage cuts at the expense of purity.

## Thank You for Listening



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